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«Northern Interindustry Company  
«The Alternative» Ltd  
For the attention of Chief Engineer  
V.I. Manykovsky

**Conclusion**  
**on the results of RAH heat exchange elements replacement in power generating unit**  
**No.3 during major repair period in 2007**

As the result of carried out works boiler gross efficiency has increased by:

$$\Delta\eta = 91.97 - 91.23 = 0.74\%$$

Boiler efficiency was increased due to the lowering of heat loss with flue gases  $q_2$  according to the following parameters:

- lowering of the cold air inleakage
- lowering of the temperature of flue gases
- increasing of the hot air temperature

The positive parameters after RAH repair in 3B boiler body where CMKA® heat exchange elements produced by Northern Interindustry Company «The Alternative» Ltd were installed are as follows:

- lowering of aerodynamic resistance that led to auxiliary power consumption reduction,
- increasing of regeneration coefficient by 2% that led to lowering of the temperature of flue gases by 12 °C and rising of the hot air temperature by 12-13 °C.

Enclosure: Table 1 «List of the main technical and economic indices of PK-41 boiler No.3 at Konakovo SDPP before and after major repair period in 2007».

Deputy Chief Engineer for Repair

A.A. Kazansky

Table 1

## List of the main technical and economic indices of PK-41 boiler No.3, at Konakovo SDPP before and after major repair period in 2007

Parameter	Dimension	before repair on June 26, 2007				after repair on January 30, 2008			
		A	B	C	D	A	B	C	D
Electrical load (not fixed)	MW	302.39				314.73			
Gas temperature before RAH	°C	340.57	344.71	331	340	335.17	338.01	335.5	339.07
Gas temperature behind RAH	°C	169	190	154.29	162.86	149.06	144.53	125.88	147.59
Air temperature behind RAH	°C	290.57	289	285	282	284.07	280.46	292.64	298.08
Air temperature before RAH	°C	31	33.29	30.29	30.29	32.45	33.14	33.3	33.92
Device gas consumption	m <sup>3</sup> /hour	37170		38270		34423		34370	
Fixed gas consumption	m <sup>3</sup> /hour	41425.37		42509.35		40664.37		40538.14	
Oxygen content in flue gases before transition zone taking into account thermal aerodynamic coefficient	%	2.4	2.02	1.875	2.067	1.60	1.56	2.30	1.32
Excess coefficient	-	1.116129	1.095785	1.088235	1.098257	1.0742268	1.072222	1.110695	1.060366
Oxygen content in flue gases behind smoke exhaust	%	7		7,27		7		7	
Excess coefficient	-	1.45		1.476547706		1.45		1.45	
Flue gases vacuum behind RAH	kgf/m <sup>2</sup>	286	283	287	284	252	250	263	258
Flue gases vacuum before RAH	kgf/m <sup>2</sup>	184	174	178	185	167	160	165	168
Air pressure before RAH	kgf/m <sup>2</sup>	205	212	257	230	187	189	209	210
Air pressure behind RAH	kgf/m <sup>2</sup>	127	120	143	144	119	120	121	123
Air inleakage into furnace	%	14.1		13.2		10.4		13.2	
Heat got by steam per the boiler drum	kcal/hour	305292661		320516726		309966865		306238004	
Combustion heat	kcal/m <sup>3</sup>	8015				7993			
Temperature of flue gases behind smoke exhaust	°C	166.57		158		153.45		147.56	
Air suction into gas duct	%	29.2		36.1		34.06		33.6	
Boiler efficiency (actual)	%	91.6		91.85		92.24		92.54	
Boiler efficiency (fixed)	%	91.09		91.37		91.82		92.13	